

# Carbon Dioxide Corrosion in Steel Pipes

A flow mixture of water and carbon dioxide (CO<sub>2</sub>) passing through a steel pipe can cause significant steel corrosion. Properties such as partial pressure of  ${\rm CO}_2$  and temperature affect the corrosion rate.

This model simulates the corrosion taking place on the steel surface of a pipe carrying CO<sub>2</sub> and water mixture. The model is based on several journal papers (Ref. 1–Ref. 3).

## Model Definition

The corrosion is investigated at an arbitrary position within a steel pipe through which a flow of dissolved CO<sub>2</sub> in water passes. A 1D model is used. No variations along the length of the pipe are considered and the interaction of the mixture with the steel is confined to the boundary layer near the steel surface. The boundary layer thickness is considered to be  $50 \mu m$ . The model geometry is shown in Figure 1.

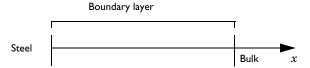


Figure 1: The model geometry comprising of the boundary layer adjacent to the steel surface.

All species are assumed to be diluted in water and the mass transport is modeled by diffusion and migration. The Tertiary Current Distribution, Nernst-Planck interface with water-based charge electroneutrality is used in the model. Carbon dioxide hydration, water dissociation, proton reduction reaction, and iron dissolution reaction are accounted for; resulting in four species (in addition to H<sup>+</sup> and OH<sup>-</sup> ions) in the model. The species and diffusion coefficients are tabulated in Table 1

TARIF I.	MODELED	SPECIES WITH	THEIR R	ESPECTIVE	DIFFLISION	COEFFICIENTS.

Species	D (m <sup>2</sup> /s)·10 <sup>-9</sup>
CO <sub>2</sub>	1.96
H <sub>2</sub> CO <sub>3</sub>	2.00
HCO <sub>3</sub>	1.11
H <sup>+</sup>	9.31
OH <sup>-</sup>	5.26
Fe <sup>2+</sup>	0.72

The Electrode Surface boundary feature is used to calculate the corrosion potential at the steel surface. The electric potential is set to 0 at the steel surface which will result in a mixed potential condition since the electrolyte potential is left to float. The initial value of the electrolyte potential is set to -0.5 V around the free corrosion potential (Ref. 2).

Fluxes of species converted in the electrochemical reactions,  $i_j/F$  (Faraday's constant = 96,485 C/mol), are applied on the steel surface where i (SI unit: A/m<sup>2</sup>) is the current density of j number of electrochemical reactions.

For all species, uniform concentrations of species in chemical equilibrium are used as initial values for concentration (Ref. 1). Concentration of CO<sub>2</sub> is set to its initial value at the outer point of the boundary layer.

## **EQUILIBRIUM REACTIONS**

The following equilibrium reactions are present in the electrolyte:

$$\begin{aligned} & \text{H}_2\text{O}(\text{l}) \Leftrightarrow \text{H}^+(\text{aq}) + \text{OH}^-(\text{aq}) & K_1 &= 6.418 \cdot 10^{-15} \\ & \text{CO}_2(\text{aq}) + \text{H}_2\text{O}(\text{aq}) \Leftrightarrow \text{H}_2\text{CO}_3(\text{aq}) & K_2 &= 2.580 \cdot 10^{-3} \\ & \text{H}_2\text{CO}_3(\text{aq}) \Leftrightarrow \text{H}^+(\text{aq}) + \text{HCO}_3^-(\text{aq}) & K_3 &= 1.251 \cdot 10^{-4} \end{aligned}$$

where  $K_1$  through  $K_3$  are the equilibrium constants at 293.15 K (Ref. 1).

The water dissociation equilibrium reaction is in-built for the Tertiary Current Distribution, Nernst–Planck interface with water-based charge electroneutrality charge transport. The other two reactions are modeled using the Equilibrium Reaction domain node; one for each reaction. The Equilibrium Reaction nodes solve for one additional degree of freedom each, where the additional degree of freedom represents the local reaction rate required in order to fulfill the equilibrium expression. The equilibrium expressions are based on the reaction stoichiometry and equilibrium constant  $K_k$  according to

$$K_k = \prod_i a(c_i)^{v_{ik}}$$

where  $c_i$  (SI unit: mol/m<sup>3</sup>) is the concentration of species i,  $v_{ik}$  the stoichiometric coefficient of species i in reaction k. The activity of a species,  $a(c_i)$  is given by dividing the concentration with 1 M.

#### **ELECTROCHEMICAL REACTIONS**

The following electrochemical reactions are present at the steel surface:

Iron dissolution

$$Fe(s) \rightarrow Fe^{2+} + 2e^{-}$$

· Proton reduction

$$H^{+} + e^{-} \rightarrow \frac{1}{2}H_{2}$$

### STUDY SETTINGS

The problem is solved with an auxiliary sweep on a stationary solver in order to investigate the impact of important parameters such as partial pressure of CO<sub>2</sub> and temperature on corrosion.

## Results and Discussion

Figure 2 displays the concentration deviation from the bulk of the four species along the boundary layer at partial pressure of CO<sub>2</sub> of 1 bar and 20°C. The concentration of iron ions is significantly higher at the steel surface due to the dissolution of iron. The deviation of carbon dioxide and bicarbonate ions show considerable hydration of the carbon

dioxide. Carbonic acid shows little variation in concentration compared to the bulk throughout the boundary layer.

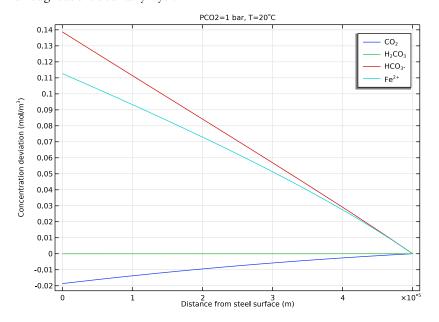


Figure 2: Deviation in concentration of the species compared to the bulk along the liquid boundary layer.

Figure 3 shows the corrosion rate of the steel surface at different partial pressures of CO<sub>2</sub> for operating temperatures ranging from 20°C to 80°C. The corrosion rate is directly proportional to the corrosion current (that is, the iron dissolution current, since no other anodic reaction is considered). Increased partial pressure of CO<sub>2</sub> and temperature increase the corrosion rate.

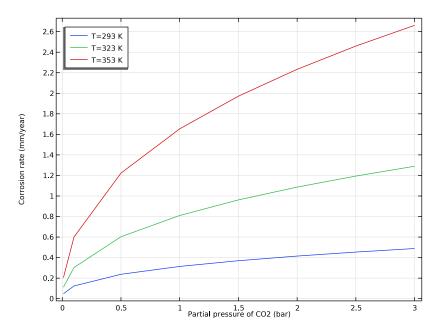


Figure 3: Corrosion rate in mm/year for different partial pressures of CO2 and operating temperatures range of 20°C-80°C.

Figure 4 and Figure 5 show the change in pH at the steel surface and bulk electrolyte, respectively, for different partial pressures of CO2 and for operating temperatures ranging from 20°C to 80°C. The higher pH is observed for lower partial pressure of CO<sub>2</sub> at both the electrode surface as well as the bulk electrolyte for all operating temperatures considered in the model. The increase in pH with an increase in temperature is observed to be more significant at the electrode surface when compared to the bulk electrolyte.

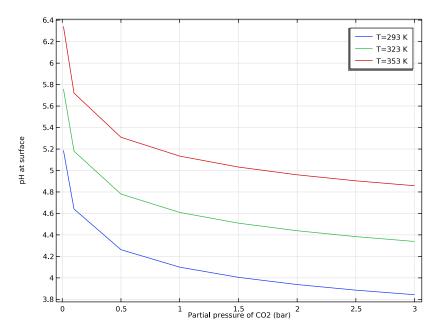


Figure 4: pH at the electrode surface for different partial pressures of  $\rm CO_2$  and operating temperatures range of  $\rm 20^oC-80^oC$ .

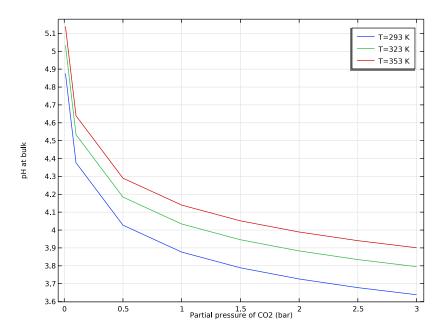


Figure 5: pH at the bulk electrolyte for different partial pressures of CO2 and operating temperatures range of 20°C-80°C.

## References

- 1. M. Nordsveen, S. Nesic, R. Nyborg, and A. Stangeland, "A Mechanistic Model for Carbon Dioxide Corrosion of Mild Steel in the Presence of Protective Iron Carbonate Films-Part 1: theory and Verification," Corrosion, vol. 59, no. 5, pp. 443-455, 2003.
- 2. S. Nesic, J. Postlethwaite, and S. Olsen, "An Electrochemical Model for Prediction of Corrosion of Mild Steel in Aqueous Carbon Dioxide Solutions," Corrosion, vol. 52, no. 4, pp. 280-294, 1996.
- 3. A. Kahyarian and S. Nesic, "On the mechanism of carbon dioxide corrosion of mild steel: Experimental investigation and mathematical modeling at elevated pressures and non-ideal solutions," Corrosion Science, vol. 173, no. 108719, pp. 1-27, 2020.

Application Library path: Corrosion\_Module/General\_Corrosion/co2\_corrosion

From the File menu, choose New.

#### NEW

In the New window, click Model Wizard.

## MODEL WIZARD

- I In the Model Wizard window, click ID.
- 2 In the Select Physics tree, select Electrochemistry>Tertiary Current Distribution, Nernst-Planck>Tertiary, Water-Based with Electroneutrality (tcd).
- 3 Click Add.
- 4 In the Number of species text field, type 4.
- 5 In the Concentrations (mol/m³) table, enter the following settings:

cC02 cH2C03 cHC03 cFe

- 6 Click Study.
- 7 In the Select Study tree, select General Studies>Stationary.
- 8 Click M Done.

#### GLOBAL DEFINITIONS

Load the model parameters from a text file.

## Parameters 1

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, locate the Parameters section.
- 3 Click Load from File.
- 4 Browse to the model's Application Libraries folder and double-click the file co2\_corrosion\_parameters.txt.

#### **GEOMETRY I**

The geometry consists of a single interval.

## Interval I (iI)

- I In the Model Builder window, under Component I (compl) right-click Geometry I and choose Interval.
- 2 In the Settings window for Interval, locate the Interval section.
- **3** In the table, enter the following settings:

Coordinates (m)		
0		
delta		

4 Click | Build Selected.

## TERTIARY CURRENT DISTRIBUTION, NERNST-PLANCK (TCD)

Start defining the physics.

## Species Charges 1

- I In the Model Builder window, under Component I (compl)>Tertiary Current Distribution, Nernst-Planck (tcd) click Species Charges 1.
- 2 In the Settings window for Species Charges, locate the Charge section.
- 3 In the  $z_{\rm cHCO3}$  text field, type -1.
- 4 In the  $z_{cFe}$  text field, type 2.

## Electrolyte I

- I In the Model Builder window, click Electrolyte I.
- 2 In the Settings window for Electrolyte, locate the Diffusion section.
- **3** In the  $D_{\rm cCO2}$  text field, type DCO2.
- **4** In the  $D_{\rm cH2CO3}$  text field, type DH2CO3.
- **5** In the  $D_{\rm cHCO3}$  text field, type DHCO3.
- **6** In the  $D_{cFe}$  text field, type DFe.
- **7** In the  $D_{\rm cH}$  text field, type DH.
- **8** In the  $D_{\rm cOH}$  text field, type DOH.

### Initial Values 1

Set the initial values to the concentration of the species in the bulk.

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- 3 In the cCO2 text field, type cCO20.

- **4** In the cH2CO3 text field, type cH2CO30.
- **5** In the *cHCO*3 text field, type cHC030.
- **6** In the cFe text field, type cFe0.
- **7** In the *phil* text field, type philo.

### Electrode Surface I

Use the Dissolving-Depositing species formulation to estimate the corrosion rate. Also, set fluxes according to the electrochemical reactions at the steel surface.

- I In the Physics toolbar, click Boundaries and choose Electrode Surface.
- 2 Select Boundary 1 only.
- 3 In the Settings window for Electrode Surface, click to expand the Dissolving-Depositing Species section.
- 4 Click + Add.
- **5** In the table, enter the following settings:

Species	Density (kg/m^3)	Molar mass (kg/mol)
s1	rho_steel	Mw_steel

#### Electrode Reaction 1

- I In the Model Builder window, click Electrode Reaction I.
- 2 In the Settings window for Electrode Reaction, locate the Stoichiometric Coefficients section.
- 3 In the n text field, type 2.
- 4 In the  $v_{cFe}$  text field, type -1.
- 5 In the Stoichiometric coefficients for dissolving-depositing species: table, enter the following settings:

Species	Stoichiometric coefficient (I)	
sl	-1	

- **6** Locate the **Equilibrium Potential** section. In the  $E_{\text{eq.ref}}(T)$  text field, type Eeq\_ref\_Fe.
- **7** Locate the **Electrode Kinetics** section. In the  $i_{0,ref}(T)$  text field, type i0\_ref\_Fe.
- **8** In the  $\alpha_a$  text field, type alphaa\_Fe.

## Electrode Surface 1

In the Model Builder window, click Electrode Surface 1.

#### Electrode Reaction 2

- I In the Physics toolbar, click \_\_\_ Attributes and choose Electrode Reaction.
- 2 In the Settings window for Electrode Reaction, locate the Equilibrium Potential section.
- **3** In the  $E_{\text{eq.ref}}(T)$  text field, type Eeq\_ref\_H2.
- **4** Locate the **Electrode Kinetics** section. In the  $i_{0,ref}(T)$  text field, type i0\_ref\_H2.
- **5** In the  $\alpha_a$  text field, type alphaa\_H2.

## Equilibrium Reaction 1

Set two equilibrium reactions.

- I In the Physics toolbar, click Domains and choose Equilibrium Reaction.
- 2 In the Settings window for Equilibrium Reaction, locate the Domain Selection section.
- 3 From the Selection list, choose All domains.
- **4** Locate the **Equilibrium Condition** section. In the  $K_{eq}$  text field, type KCO2H.
- **5** Locate the **Stoichiometric Coefficients** section. In the  $v_{cCO2}$  text field, type -1.
- **6** In the  $v_{cH2CO3}$  text field, type 1.

## Equilibrium Reaction 2

- I In the Physics toolbar, click Domains and choose Equilibrium Reaction.
- 2 In the Settings window for Equilibrium Reaction, locate the Domain Selection section.
- 3 From the Selection list, choose All domains.
- **4** Locate the **Equilibrium Condition** section. In the  $K_{\rm eq}$  text field, type KH2CO3.
- **5** Locate the **Stoichiometric Coefficients** section. In the  $v_{cH2CO3}$  text field, type -1.
- **6** In the  $v_{cHCO3}$  text field, type 1.
- 7 In the  $v_{cH}$  text field, type 1.

#### Concentration I

Set bulk concentrations at the rightmost boundary.

- I In the Physics toolbar, click Boundaries and choose Concentration.
- 2 Select Boundary 2 only.
- 3 In the Settings window for Concentration, locate the Concentration section.
- **4** Select the **Species cCO2** check box.
- **5** Select the **Species cFe** check box.
- **6** In the  $c_{0,\text{cCO}2}$  text field, type cCO20.
- **7** In the  $c_{0,cFe}$  text field, type cFe0.

#### MESH I

Build a user-defined mesh with a maximum element size in the domain of 1e-6 and at the leftmost boundary 1e-7.

- I In the Model Builder window, under Component I (compl) click Mesh I.
- 2 In the Settings window for Mesh, locate the Sequence Type section.
- 3 From the list, choose User-controlled mesh.

#### Size

- I In the Model Builder window, under Component I (compl)>Mesh I click Size.
- 2 In the Settings window for Size, locate the Element Size section.
- 3 Click the **Custom** button.
- 4 Locate the Element Size Parameters section. In the Maximum element size text field, type 1e-6.

#### Size 1

- I In the Model Builder window, right-click Edge I and choose Size.
- 2 In the Settings window for Size, locate the Geometric Entity Selection section.
- 3 From the Geometric entity level list, choose Boundary.
- 4 Select Boundary 1 only.
- **5** Locate the **Element Size** section. Click the **Custom** button.
- 6 Locate the Element Size Parameters section.
- 7 Select the Maximum element size check box. In the associated text field, type 1e-7.
- 8 Click **Build Selected**.

#### STUDY I

- I In the Model Builder window, click Study I.
- 2 In the Settings window for Study, locate the Study Settings section.
- 3 Clear the Generate default plots check box.

#### Parametric Sweep

Use parametric sweep to investigate the impact of CO2 partial pressure and temperature.

- I In the Study toolbar, click Parametric Sweep.
- 2 In the Settings window for Parametric Sweep, locate the Study Settings section.
- 3 Click + Add twice.

**4** In the table, enter the following settings:

Parameter name	Parameter value list	Parameter unit	
PCO2 (Partial pressure of CO2 in bar)	0.01 0.1 range(0.5,0.5, 3)		
T (Operating temperature)	293.15[K] 323.15[K] 353.15[K]	К	

5 From the Sweep type list, choose All combinations.

Solution I (soll)

- I In the Study toolbar, click Show Default Solver.
- 2 In the Model Builder window, expand the Solution I (soll) node.
- 3 In the Model Builder window, under Study 1>Solver Configurations>Solution 1 (sol1) click Stationary Solver 1.
- 4 In the Settings window for Stationary Solver, locate the General section.
- 5 In the Relative tolerance text field, type 1e-6.
- 6 In the Study toolbar, click **Compute**.

#### RESULTS

The following steps reproduces the plots from the Results and Discussion section.

## Concentrations

- I In the Home toolbar, click Add Plot Group and choose ID Plot Group.
- 2 In the Settings window for ID Plot Group, type Concentrations in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Study I/Solution I (soll).
- 4 From the Parameter selection (PCO2) list, choose Last.
- 5 From the Parameter selection (T) list, choose First.
- **6** Click to expand the **Title** section. From the **Title type** list, choose **Manual**.
- 7 In the Title text area, type PCO2=1 bar, T=20<sup>\circ</sup>C.
- 8 Locate the Plot Settings section.
- 9 Select the x-axis label check box. In the associated text field, type Distance from steel surface (m).
- 10 Select the y-axis label check box. In the associated text field, type Concentration deviation (mol/m<sup>3</sup>).

### Line Graph 1

- I Right-click Concentrations and choose Line Graph.
- 2 In the Settings window for Line Graph, locate the Selection section.
- 3 From the Selection list, choose All domains.
- 4 Locate the y-Axis Data section. In the Expression text field, type cC02-cC020.
- 5 Click to expand the **Title** section. From the **Title type** list, choose **None**.
- 6 Locate the x-Axis Data section. From the Parameter list, choose Expression.
- **7** In the **Expression** text field, type x.
- **8** Click to expand the **Legends** section. Select the **Show legends** check box.
- 9 From the Legends list, choose Manual.
- **IO** In the table, enter the following settings:

# Legends CO<sub>2</sub>

II Right-click Line Graph I and choose Duplicate.

## Line Graph 2

- I In the Model Builder window, click Line Graph 2.
- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- 3 In the Expression text field, type cH2C03-cH2C030.
- **4** Locate the **Legends** section. In the table, enter the following settings:

## Legends H<sub>2</sub>CO<sub>3</sub>

5 Right-click Line Graph 2 and choose Duplicate.

#### Line Graph 3

- I In the Model Builder window, click Line Graph 3.
- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- **3** In the **Expression** text field, type cHC03-cHC030.
- **4** Locate the **Legends** section. In the table, enter the following settings:

# Legends HCO<sub>3</sub><sup>-</sup>

**5** Right-click **Line Graph 3** and choose **Duplicate**.

### Line Graph 4

- I In the Model Builder window, click Line Graph 4.
- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- 3 In the Expression text field, type cFe-cFe0.
- **4** Locate the **Legends** section. In the table, enter the following settings:

## Legends Fe<sup>2+</sup>

5 In the Concentrations toolbar, click Plot.

#### Corrosion rate

- I In the Home toolbar, click **Add Plot Group** and choose ID Plot Group.
- 2 In the Settings window for ID Plot Group, type Corrosion rate in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Study I/Solution I (soll).
- 4 Locate the Title section. From the Title type list, choose None.
- **5** Locate the **Plot Settings** section.
- 6 Select the x-axis label check box. In the associated text field, type Partial pressure of CO2 (bar).
- 7 Select the y-axis label check box. In the associated text field, type Corrosion rate (mm/year).

#### Point Grabh 1

- I Right-click Corrosion rate and choose Point Graph.
- **2** Select Boundary 1 only.
- 3 In the Settings window for Point Graph, click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)> Tertiary Current Distribution, Nernst-Planck>Dissolving-depositing species>tcd.vbtot -Total electrode growth velocity - m/s.
- 4 Locate the y-Axis Data section. From the Unit list, choose mm/yr.
- 5 Locate the x-Axis Data section. From the Axis source data list, choose PCO2.
- **6** From the **Parameter** list, choose **Expression**.
- 7 In the Expression text field, type PC02.
- 8 Click to expand the **Legends** section. Select the **Show legends** check box.
- 9 From the Legends list, choose Evaluated.
- 10 In the Legend text field, type T=eval(T) K.

#### Corrosion rate

- I In the Model Builder window, click Corrosion rate.
- 2 In the Settings window for ID Plot Group, locate the Legend section.
- 3 From the Position list, choose Upper left.
- 4 In the Corrosion rate toolbar, click Plot.
- **5** Right-click **Corrosion rate** and choose **Duplicate**.

### bH at surface

- I In the Model Builder window, under Results click Corrosion rate I.
- 2 In the Settings window for ID Plot Group, type pH at surface in the Label text field.
- 3 Locate the Plot Settings section. In the y-axis label text field, type pH at surface.

## Point Graph 1

- I In the Model Builder window, expand the pH at surface node, then click Point Graph I.
- 2 In the Settings window for Point Graph, locate the y-Axis Data section.
- 3 In the Expression text field, type tcd.pH.

## pH at surface

- I In the Model Builder window, click pH at surface.
- 2 In the Settings window for ID Plot Group, locate the Legend section.
- **3** From the **Position** list, choose **Upper right**.
- 4 In the pH at surface toolbar, click Plot.
- **5** Right-click **pH at surface** and choose **Duplicate**.

## bH at bulk

- I In the Model Builder window, under Results click pH at surface I.
- 2 In the Settings window for ID Plot Group, type pH at bulk in the Label text field.
- 3 Locate the Plot Settings section. In the y-axis label text field, type pH at bulk.

## Point Graph 1

- I In the Model Builder window, expand the pH at bulk node, then click Point Graph I.
- 2 In the Settings window for Point Graph, locate the Selection section.
- **3** Click to select the **Activate Selection** toggle button.
- 4 In the list, select 1.
- **5** Select Boundary 2 only.
- 6 In the pH at bulk toolbar, click Plot.